A First Course on Kinetics and Reaction Engineering Unit 31. Back-Mixing in a PFR via Recycle

Definitions

Recycle - split the effluent from a process and mix part of it into the feed to that process.

Nomenclature

 C_i molar concentration of species *i*

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- $\hat{C}_{p,i}$ constant pressure specific molar heat capacity of species *i*
- R_R recycle ratio
- Т temperature; a subscript denotes the associated stream
- Ŵ volumetric flow rate; a subscript denotes the associated stream
- fi fractional conversion of species *i*, an additional subscript indicates whether it is defined for the overall process or for the reactor only
- molar flow rate of species *i*; an additional subscript denotes the associated stream **n**i

Equations

$$R_{R} = \frac{\dot{V}_{r}}{\dot{V}_{d}} = \frac{\dot{n}_{total,r}}{\dot{n}_{total,d}} = \frac{\dot{n}_{i,r}}{\dot{n}_{i,d}}$$
(31.1)

$$\dot{n}_{i,b} = \dot{n}_{i,a} + \dot{n}_{i,r} = \dot{n}_{i,a} + R_R \dot{n}_{i,d}$$
(31.2)

$$\dot{n}_{i,c} = \dot{n}_{i,d} + \dot{n}_{i,r} = \dot{n}_{i,d} + R_R \dot{n}_{i,d} = (1 + R_R) \dot{n}_{i,d}$$
(31.3)

$$\dot{n}_{i,d} = \frac{\dot{n}_{i,c}}{1 + R_R}$$
(31.4)

$$\dot{n}_{i,a} + \frac{R_R \dot{n}_{i,c}}{1 + R_R} - \dot{n}_{i,b} = 0$$
(31.5)

$$\sum_{\substack{i=all\\species}} \dot{n}_{i,a} \int_{T_a}^{T_b} \hat{C}_{p,i} dT + \sum_{\substack{i=all\\species}} \dot{n}_{i,r} \int_{T_c(=T_r)}^{T_b} \hat{C}_{p,i} dT = 0$$
(31.6)

$$f_{i,pass} = \frac{\dot{n}_{i,b} - \dot{n}_{i,c}}{\dot{n}_{i,b}}$$
(31.7)

$$f_{i,overall} = \frac{\dot{n}_{i,a} - \dot{n}_{i,d}}{\dot{n}_{i,a}}$$
(31.8)

$$C_i = \frac{\dot{n}_i}{\dot{V}} \tag{31.9}$$

$$C_{i} = \frac{\dot{n}_{i}}{\dot{V}_{b}} = \frac{\dot{n}_{i}}{\dot{V}_{a} + \dot{V}_{r}} = \frac{\dot{n}_{i}}{\dot{V}_{a} + R_{R}\dot{V}_{d}} = \frac{\dot{n}_{i}}{\dot{V}_{a}(1 + R_{R})}$$
(31.10)