

# A First Course on Kinetics and Reaction Engineering

## Unit 22. Analysis of Steady State CSTRs

### Nomenclature

$\Delta H_j$	heat of reaction $j$
$v_{i,j}$	stoichiometric coefficient of species $i$ in reaction $j$ ; value is positive for products and negative for reactants
$A$	heat transfer area between the reaction volume and the heat transfer fluid
$C_i$	molar concentration of species $i$
$\tilde{C}_{p,e}$	mass-specific heat capacity of the heat transfer fluid
$\hat{C}_{p,i}$	constant pressure specific molar heat capacity of species $i$
$P$	pressure; a subscripted $i$ denotes the partial pressure of species $i$
$\dot{Q}$	net heat input into a reactor through its walls or the walls of a submerged cooling coil
$R$	ideal gas constant
$S_{i/j}$	selectivity (mol $i$ per mol $j$ )
$T$	temperature; a superscripted 0 denotes the inlet temperature; a subscripted $e$ denotes the (external) temperature of the heat transfer media
$U$	overall heat transfer coefficient for heat transfer through the wall of a tubular reactor
$V$	reaction volume
$\dot{V}$	volumetric flow rate; a superscripted zero denotes the value at the reactor inlet
$\dot{W}$	net rate at which mechanical work is done by a reactor system on its surroundings through shafts and moving boundaries
$f_i$	fractional conversion of species $i$ or a mathematical function that does not include derivatives or integrals
$\dot{m}$	mass flow rate of heat transfer fluid
$\dot{n}_i$	molar flow rate of species $i$ ; a superscripted zero denotes the value at the reactor inlet
$r_j$	the generalized rate of reaction $j$

### Equations

$$0 = \dot{n}_i^0 - \dot{n}_i + V \sum_{\substack{j=\text{all} \\ \text{reactions}}} v_{i,j} r_j \quad (22.1)$$

$$0 = \sum_{\substack{i=all \\ species}} \left( \dot{n}_i^0 \int_{T^0}^T \hat{C}_{pi} dT \right) + V \sum_{\substack{j=all \\ reactions}} r_j \Delta H_j(T) - \dot{Q} + \dot{W} \quad (22.2)$$

$$0 = \dot{m} \tilde{C}_{p,e} (T_e^0 - T_e) - \dot{Q} \quad (22.3)$$

$$\dot{Q} = UA(T_e - T) \quad (22.4)$$

$$P_i = \frac{\dot{n}_i}{\sum_{k = \text{all species}} \dot{n}_k} P \quad (22.5)$$

$$C_i = \frac{\dot{n}_i}{\dot{V}} \quad (22.6)$$

$$\dot{V} = \dot{V}^0 \quad (\text{constant density liquid}) \quad (22.7)$$

$$\dot{V} = \frac{RT \left( \sum_{k = \text{all species}} \dot{n}_k \right)}{P} \quad (\text{ideal gas}) \quad (22.8)$$

$$\dot{n}_i = \dot{n}_i^0 (1 - f_i) \quad (22.9)$$

$$\dot{n}_i = S_{i/j} \dot{n}_j \quad (22.10)$$

$$\begin{aligned} 0 &= f_1(z_1, z_2, \dots, z_n) \\ 0 &= f_2(z_1, z_2, \dots, z_n) \\ &\vdots \\ 0 &= f_n(z_1, z_2, \dots, z_n) \end{aligned} \quad (22.11)$$